Amend the paragraph at column 2, lines 30-31, as follows:

B2 (Amended) According to another embodiment of the present invention is a method of preparing 2,6-dimethylnaphthalene.

Amend the paragraph at column 2, lines 34-50, as follows:

B3 (Amended) These and other objects of the present invention are made possible by a method of producing 2,6-dialkylnaphthalene from a feedstock which contains at least one component selected from the group consisting of dialkylnaphthalene isomers, monoalkylnaphthalene isomers and naphthalene comprising the following steps:

I. separating a feedstock into naphthalene, monoalkylnaphthalene, and dialkylnaphthalene fractions;

II. separating and purifying 2,6-dialkylnaphthalene from said dialkylnaphthalene fraction of step I;

III. alkylating said monoalkylnaphthalene fraction of step I with an alkylating agent to produce dialkylnapthalene;

IV. transalkylating said naphthalene fraction of step I and a dialkylnaphthalene fraction, after 2,6-dialkylnaphthalene is separated therefrom in step II, to produce monoalkylnaphthalene, and isomers of dialkylnaphthalene.

Amend the paragraph at column 4, lines 10-17, as follows:

(Amended) The conditions of alkylation include a temperature of about 0 to 500°C., and preferably 240 and 450°C., and a pressure of between 0 to 250 atmospheres and preferably 1 to 50 atmospheres. The mole ratio of alkylating agent to feed of monoalkylnaphthalene or naphthalene can be from about 20:1 to 1:20, preferably from 10:1 to 1:10. The reaction is suitably accomplished utilizing a feed space velocity of about 0.1 to 10.0 hr^{-1}.

B4

Amend the paragraph at column 5, lines 16-35, as follows:

(Amended) The method involves injecting the slurry or liquid of the temperature of 70 to 120°C., preferably 80 to 100°C., into a high pressure vessel for conducting a crystallization under high pressure; adiabatically pressurizing the vessel to a pressure of from 300 to 4,000 kgf/cm^2, preferably 500 to 2,000 kgf/cm^2 to increase the quantity, i.e. the amount of 2,6-dialkylnaphthalene crystals, whereby coexistence of solid-liquid phases exist at the high pressure conditions; discharging the liquid phase component from the high pressure vessel, the discharging being conducted under pressure, to increase the ratio of the solid phase relative to the liquid phase within the vessel; lowering the pressure of the residual liquid phase so as to dissolve partially and purify the product; discharging the residual liquid phase by applying pressure to the solid phase within the high pressure vessel whereby a 2,6-dialkylnaphthalene crystal block having a high purity is obtained with the high pressure vessel. By this technique, a purity of 2,6-dialkylnaphthalene (e.g. 2,6-dimethylnaphthalene) of ≥98% by weight, preferably ≥99% by weight may be obtained.

B5